



Metal vapour derived supported rhodium nanoparticles in the synthesis of β -lactams and β -lactones derivatives

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ABSTRACT

Functionalised β -lactones and β -lactams were prepared starting from propargyl alcohols and propargyl tosyl amides by means of efficient silylcarbocyclisation reactions catalysed by rhodium nanoparticles derived from mesitylene-solvated Rh atoms (Metal Vapour Synthesis technique, MVS) and deposited on inorganic (C, γ -Al₂O₃ Fe₂O₃) and organic matrices (PBI). All the MVS supported nanoclusters resulted more active than the analogous commercial Rh/C and Rh/ γ -Al₂O₃, as well as homogeneous Rh₄(CO)₁₂ used as reference catalyst. In particular, metal vapour derived Rh/C afforded the β -lactones and β -lactams in high yields and chemoselectivity. Preliminary investigations on the nature of the real active metal species involved in the catalytic process showed that rhodium(0) naked nanoparticles are leached by the support. The high catalytic activity encountered with Rh/C could be ascribed to the easy leaching of metal nanoparticles from carbon into solution. Indeed, the presence of a more polar matrix determined a minor catalytic efficiency probably due to a stronger interaction between the metal and the support. Therefore MVS Rh/C species represents a source, stable with ageing at room temperature, of highly active metal nanoparticles.

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1. Introduction

Four-membered monocyclic heterocycles have received little interest from the chemical community compared to the higher homologous counter parts. Between β -lactams and β -lactones, the greatest attention was obviously paid to the first ones (also called azetidines) since the β -lactam ring is the key of one of the most widely employed class of antibacterial agents, the β -lactam antibiotics which are distinguished by good tolerance and therapeutic safety (e.g. Tigemonam[®]) [1–5]. Among β -lactams, the α -methylene- β -lactam unit is a common structural feature included in potent β -lactamase inhibitors such as asparenomyins and penicillanic acids [6–17].

On the contrary to what reported for β -lactams, β -lactones (2-oxetanones) have only recently emerged as important synthetic targets. Indeed, they have been studied as enzymes inhibitors [18–29] and have been tested in the treatment of infections generated by bacteria and viruses (i.e. human cytomegalovirus, human herpesvirus and Kaposi's sarcoma herpesvirus) [30–32]. In the field

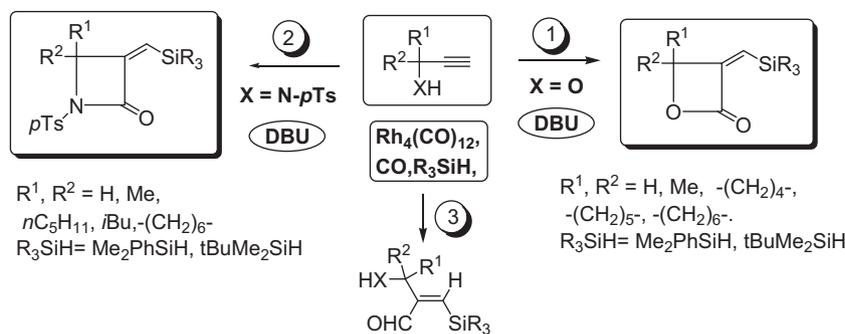
of β -lactones, α -methylene- β -lactones (3-methyleneoxetan-2-ones) were nearly unknown molecules until the late '80s. This is especially puzzling in view of the high degree of functionality contained in this heterocyclic system, which should lend itself to diversified synthetic applications [33–38].

Considering the synthetic value of β -lactams [39–41] and β -lactones [42], it is not surprising that many methods have been developed to achieve selective and efficient syntheses [43–45]. In particular, in 1990 Matsuda and co-workers [46] reported the first example of rhodium-catalysed silylcarbocyclisation of propargyl alcohols that generated α -(trialkylsilyl)methylene- β -lactones in good yields, provided that DBU and a suitable hydrosilane were used (Scheme 1, route 1). Otherwise, silylformylation by-products, derived from the direct addition of CO and silane to the triple bond, may be observed (Scheme 1, route 3).

A year later the same group published [47] the first application of the silylcarbocyclisation process to the synthesis of silylated α -methylene- β -lactams (Scheme 1, route 2) starting from easily available propargylamine derivatives.

The silylcarbocyclisation reactions are generally performed in the presence of a catalytic amount of rhodium based homogeneous species such as Rh₄(CO)₁₂ [38,48–52]. No examples of the use of heterogeneous catalysts are known though they would allow

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Scheme 1.

simpler recovery and easier purification of the product, possible recycle of the catalyst and could assure a higher thermal stability of the catalytic species.

In the field of heterogeneous catalysis, the use of supported nanoparticles represents a modern approach which takes advantage from the high reactivity of very small metal clusters. Innovative procedures have been developed to attain effective tailoring of the size of the metal particles. Successful results have been obtained employing chemical vapour deposition and thermal, photochemical, or sonochemical decomposition of organometallic complexes on a suitable matrix. All these methods afford the metal nanoparticles with good reproducibility and narrow size distributions, but the precursors, i.e. the organometallic species, may not always be easily available.

An alternative versatile methodology is the so-called Metal Vapour Synthesis (MVS) technique which is based on the formation of “solvated metal atoms” (SMA), i.e. solvent stabilized metal nanoclusters obtained by co-condensation of metal vapours with organic ligands (mesitylene, toluene, acetone...). SMA have been employed as catalytic precursors in a wide range of reactions such as hydrogenation [53–57], hydroformylation [58–60], hydrosilylation [61–66] and carbon–carbon coupling [67–70].

Recently we have reported a qualitative evaluation of the catalytic properties of rhodium supported nanoparticles, obtained from Rh/mesitylene SMA solutions, in the silylcarbocyclisation of propargyl amines and alcohols [71].

Prompted by the promising data obtained, we decided to deeply investigate the factors that influence the catalytic performances of rhodium SMA derived species in synthesis of α -methylene- β -lactams and α -methylene- β -lactones. Since the silylformylation is a common side reaction of the silylcarbocyclisation process, for this paper we started our investigation testing the activity of rhodium supported nanoparticles in the silylformylation of simple and functionalised acetylenes. As a matter of fact, we have previously described [72] that solvated rhodium atoms, prepared by the metal vapour synthesis technique, promoted the silylformylation reaction of variously substituted alkynes with catalytic activities comparable with and even higher than more common species such as $\text{Rh}_4(\text{CO})_{12}$.

Subsequently, the activity of the supported Rh-SMA was exhaustively evaluated in the silylcarbocyclisation of propargyl derivatives.

2. Results and discussion

2.1. Preparation of the catalysts

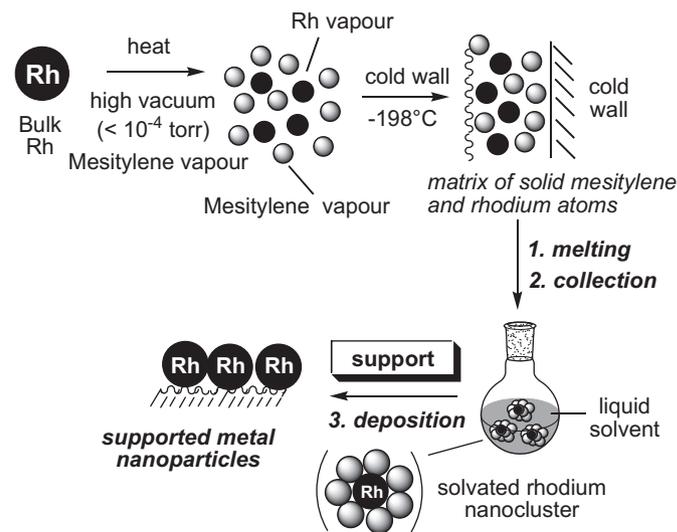
Rhodium nanoparticles were generated by means of the MVS technique. According to previously described experimental procedures [73], Rh and mesitylene were vaporised under vacuum and

deposited on the frozen walls (-196°C) of a glass reactor, generating a red-brown matrix. During the warm-up stage from -196 to -30°C the matrix melted, and nucleation and growth processes of the metal particles took place leading to rhodium(0) nanoclusters weakly stabilized by the mesitylene molecules, the so-called “solvated metal atoms” (SMA) (Scheme 2, steps 1 and 2) [74]. The obtained Rh/mesitylene solution was employed directly as source of metal nanoparticles in the carbonylation reactions.

The supported catalysts Rh/C and Rh/ γ - Al_2O_3 (Table 1 entries 3 and 4) were prepared by simple addition of the Rh/SMA to the chosen supports till decolourisation of the solution occurred, which was indicative of the complete deposition of the rhodium particles on the matrices (Scheme 2, step 3) [74]. The catalysts thus obtained were ready for use without any pre-activation step.

The morphology of all the supported nanoparticles was investigated by means of high resolution transition electron microscopy (HR-TEM) (Fig. 1 and Table 1). The particle size distribution and the mean diameter of the nanoparticles of Rh/C and Rh/ γ - Al_2O_3 prepared via MVS technique were compared with those of commercially available samples. As reported in Table 1 (entries 1 and 2) and in Fig. 1(a) and (b), the analysis of the metal particles of the commercial Rh/C and Rh/ γ - Al_2O_3 (5% Rh w/w) systems showed the presence of rhodium clusters with a broad size distribution lying in the 1.5–14 nm range and average diameters of 3.5 and 7.1 nm.

The HR-TEM analysis of the corresponding MVS catalysts (Fig.1(c) and (d), Table 1, entries 3 and 4) indicated the presence of



Scheme 2.

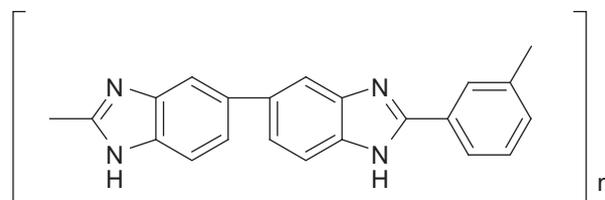
Table 1
Rhodium catalysts.

No.	Catalyst	Metal loading %w/w	Type	d_m (mean diameter, nm) ^a	Particles size distribution (nm) ^a
1	Rh/C	5	Comm.	3.5	1.5–6.0
2	Rh/Al ₂ O ₃	5	Comm.	7.1	1.5–14.0
3	Rh/C	1	MVS	2.4	1.2–4.4
4	Rh/Al ₂ O ₃	1	MVS	2.1	1.0–4.0
5	Rh/Fe ₂ O ₃	0.98	MVS	≤1	–
6	Rh/PBI	0.98	MVS	2.2	1.7–3.2

^a Determined by HR-TEM analysis.

supported rhodium particles smaller than the commercial samples, having a size distribution in a narrower range, 1.0–4.4 nm, and mean diameters of 2.4 and 2.1 nm, respectively. In these cases, moreover, two additional considerations have to be made: the former is that HR-TEM does not have a high sensitivity in revealing particles smaller than 1 nm in size, and the latter is that the occurrence of aggregation phenomena of sub-nanometric metal particles under the electron beam during HR-TEM observation cannot be excluded. As a consequence the real mean size of MVS Rh particles could be even smaller.

In order to investigate the effect of a highly polar inorganic or organic matrix on the reactivity and selectivity of the metal nanoclusters, two more supported rhodium species were prepared starting from the Rh/SMA solution: Rh/Fe₂O₃ (0.98% w/w) and

**Fig. 2.** Structure of polybenzoimidazole (PBI).

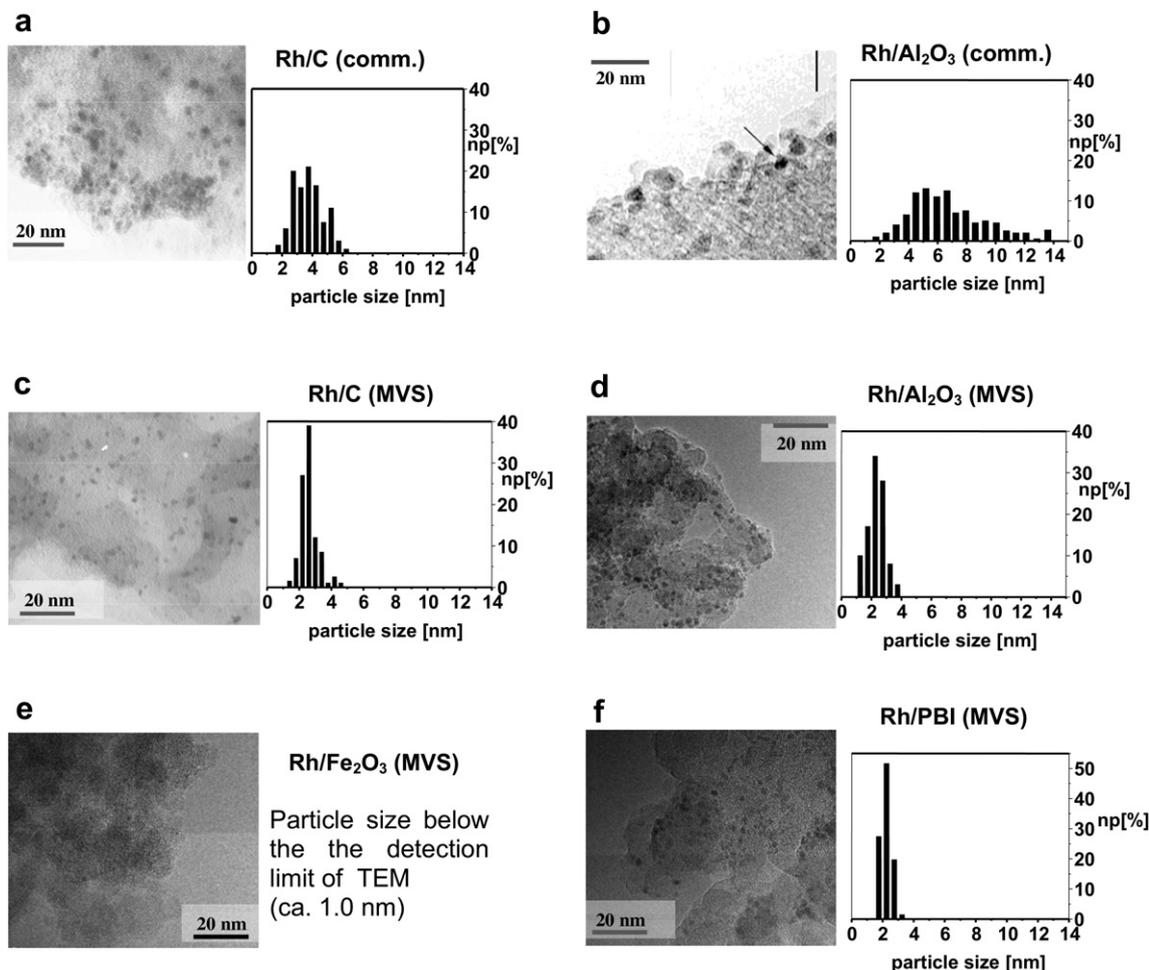
Rh/PBI (polybenzoimidazole, Fig. 2) [75], (0.98% w/w), (Fig. 1(e) and (f), Table 1, entries 5 and 6).

For Rh/PBI a statistical evaluation of the size of the Rh particles was carried out and very narrow particle size distributions were obtained: 1.7–3.2 nm. Rh particles were rather small and well dispersed with a more abundant population around 2.2 nm (Table 1, entry 6 and Fig. 1(f)).

As far as Rh/Fe₂O₃ the size of the Rh particles could not be determined since the size of the particles resulted near or less than the detection limit of the TEM technique – 1 nm. However, the metal particles seemed to be well dispersed on the support surface.

2.2. Silylformylation of terminal alkynes

The catalytic activity of MVS and commercial supported rhodium species was initially tested in the silylformylation reaction

**Fig. 1.** HR-TEM micrographs and histograms of particle size distributions of rhodium supported nanoparticles: (a) Rh/C (comm.); (b) Rh/ γ -Al₂O₃ (comm.); (c) Rh/C (MVS); (d) Rh/ γ -Al₂O₃ (MVS); (e) Rh/Fe₂O₃ (MVS); (f) Rh/PBI (MVS).

of 1-hexyne (**1a**) and dimethylphenylsilane (**2a**) chosen as model substrates (Scheme 3, Table 2).

In a typical experiment, equimolar amounts of the alkyne and Me_2PhSiH were reacted in the presence of 0.1 mol% of the rhodium catalyst with respect to the silane, in a 25 mL stainless steel autoclave pressurised to 10 atm of carbon monoxide. The reaction mixture was stirred at room temperature for the times reported in Table 2 (entries 1–8).

All the MVS rhodium species were able to catalyse the silylformylation of 1-hexyne with high chemo- and stereoselectivity, affording (*Z*)-1-(dimethylphenylsilyl)-formyl-1-hexene **3aa** exclusively.

The specific activity of the catalysts SA (calculated as $[\text{mmol}(\text{-silane})/\text{mgat Rh} \cdot \text{time of reaction(h)}] \cdot \text{conv.}\%$) resulted however dependent on the nature of the support.

While both commercial Rh/C and Rh/ $\gamma\text{-Al}_2\text{O}_3$ where almost inert (Table 2, entries 7 and 8), the supported MVS catalysts showed appreciable to excellent SA (Table 2, entries 3–6). In particular the catalytic activity of Rh/C (MVS) was comparable to the Rh/mesitylene precursor solution and even higher than $\text{Rh}_4(\text{CO})_{12}$ (Table 2, entry 3 vs. entries 2 and 1), commonly used as homogeneous catalyst in this reaction [72].

The particle sizes obtained from the HR-TEM analysis (Table 1, entries 1,2 vs. 3,4) can possibly account for the different catalytic behaviour: the smaller the nanoparticles are, the higher the specific activity is (Table 2 entries 3,4 vs. 7,8). Moreover, the presence of the carbon instead of alumina as inert support determines an improvement in the catalyst efficiency, as it is evident from the data reported in Table 2 (entry 3 vs. 4). This effect could be reasonably related to the polarity of $\gamma\text{-Al}_2\text{O}_3$ which could cause an increased stabilization of rhodium particles and a subsequent reduction of

reactivity. This observation was confirmed by using Rh/ Fe_2O_3 and Rh/PBI as catalytic precursors (Table 2, entries 5 and 6). Indeed, in these cases an even lower conversion of the reagents (around 40%) was observed.

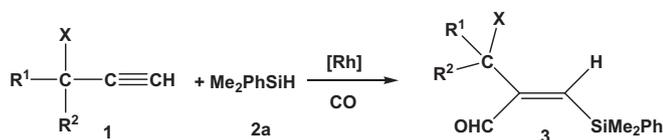
The presence of a functional group such as OH (Table 2, entries 9 and 10) did not affect the reaction path: the supported Rh/C (MVS) promoted the formation of the functionalised aldehyde **3ba** with good selectivity and specific activity similar to $\text{Rh}_4(\text{CO})_{12}$.

2.3. Silylcarbocyclisation of propargyl alcohols: synthesis of β -lactones

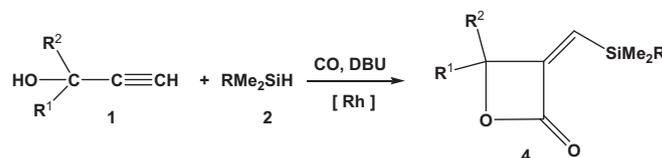
At the beginning of this study a preliminary investigation on the reactivity of MVS rhodium catalysts in the silylcarbocyclisation of a monosubstituted propargyl alcohol was carried out (Scheme 4, Table 3, entries 1–5). The reactions were performed at 100 °C for 4 h, employing 3 mmol of hydrosilane, 3 mmol of alkyne, 3×10^{-3} mmol of Rh, 3 mL of CH_2Cl_2 and 0.3 mmol of DBU under CO atmosphere (30 atm). Initially, *t*-Bu Me_2SiH **2b** was reacted with the alcohol since it is known that the silylcarbocyclisation reaction is favoured by the presence of bulky substituents on the reagents.

Rh/mesitylene solution showed an excellent catalytic performance in the synthesis of the β -lactone **4cb** which was generated with high chemoselectivity (Table 3, entry 2). When the same reactions was carried out in the presence of Rh/C, as expected, a lower reaction rate was observed (Table 3, entry 3); however the supported catalyst resulted more active and selective towards the formation of the lactone ring than $\text{Rh}_4(\text{CO})_{12}$ used as reference catalyst (Table 3, entry 3 vs. 1).

It is important to notice that the supported derived catalyst Rh/C is stable at room temperature and can be handled at open air, allowing an easy experimental procedure, while Rh/mesitylene



Scheme 3.



Scheme 4.

Table 2
Rhodium catalysts in the silylformylation of terminal alkynes.

Entry	1	R ¹	R ²	X	[Rh]	t (h)	3	Conv. (%) ^a	Sel. ^a (%)	SA ^b
1 ^c	a	<i>n</i> -Pr	H	H	$\text{Rh}_4(\text{CO})_{12}$ ^d	6	aa	98	96	41
2 ^c	a	<i>n</i> -Pr	H	H	Rh/mesitylene ^{d,e}	6	aa	91	92	152
3 ^c	a	<i>n</i> -Pr	H	H	Rh/C (MVS) ^e	6	aa	81	94	135
4 ^c	a	<i>n</i> -Pr	H	H	Rh/ $\gamma\text{-Al}_2\text{O}_3$ (MVS) ^e	6	aa	62	98	103
5 ^c	a	<i>n</i> -Pr	H	H	Rh/ Fe_2O_3 (MVS) ^e	6	aa	43	97	72
6 ^c	a	<i>n</i> -Pr	H	H	Rh/PBI (MVS) ^e	6	aa	41	96	68
7 ^c	a	<i>n</i> -Pr	H	H	Rh/ $\gamma\text{-Al}_2\text{O}_3$ (comm.)	8	aa	0	0	—
8 ^c	a	<i>n</i> -Pr	H	H	Rh/C (comm.)	8	aa	12	97	15
9 ^f	b	Me	Et	OH	$\text{Rh}_4(\text{CO})_{12}$	24	ba	86	85	9
10 ^f	b	Me	Et	OH	Rh/C (MVS) ^e	24	ba	30	85	12

^a Determined by GLC and ¹H NMR spectroscopic analysis of the reaction mixture after work up.

^b SA: $[\text{mmol}(\text{silane})/\text{mgat Rh} \cdot \text{time of reaction(h)}] \text{ conv.}\%$.

^c Reaction conditions: 2 mmol of Me_2PhSiH , 2 mmol of 1-hexyne, 2×10^{-3} mmol of Rh, 2 mL of toluene, rt, 10 atm CO; hydrosilylation by-products were detected by ¹H NMR spectroscopy.

^d See Ref. [72].

^e Catalysts prepared according to the metal vapour synthesis technique.

^f Reaction conditions: 3 mmol of Me_2PhSiH , 3 mmol of alkyne, 3×10^{-3} mmol of Rh, 3 mL of CH_2Cl_2 , 100 °C, 20 atm CO; small amounts of (*E*)-isomers were detected by ¹H NMR spectroscopy.

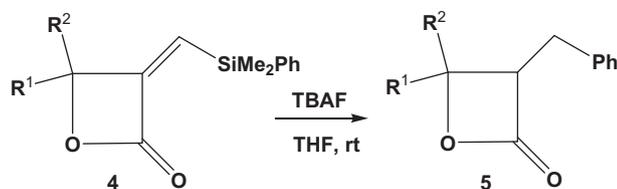
Table 3
Silylcarbocyclisation of propargyl alcohols.

Entry ^a	1	R ¹	R ²	2	R	[Rh]	t (h)	4	Conv. ^b (%)	Sel. ^b (%)	SA ^c
1	c	<i>n</i> -Pr	H	b	<i>t</i> Bu	$\text{Rh}_4(\text{CO})_{12}$	4	cb	80	66	50
2	c	<i>n</i> -Pr	H	b	<i>t</i> Bu	Rh/mesitylene	4	cb	95	87	237
3	c	<i>n</i> -Pr	H	b	<i>t</i> Bu	Rh/C (MVS)	4	cb	53	71	132
4	c	<i>n</i> -Pr	H	a	Ph	Rh/C (MVS)	4	cb	95	48	237
5	c	<i>n</i> -Pr	H	a	Ph	$\text{Rh}_4(\text{CO})_{12}$	4	cb	100	36	62
6	b	Me	Et	a	Ph	$\text{Rh}_4(\text{CO})_{12}$	4	ba	100	93	—
7	b	Me	Et	a	Ph	Rh/C (MVS)	4	ba	100	90	—
8	b	Me	Et	a	Ph	$\text{Rh}_4(\text{CO})_{12}$	1.5	ba	94	95	157
9	b	Me	Et	a	Ph	Rh/C (MVS)	1.5	ba	87	92	580
10	b	Me	Et	a	Ph	Rh/ Fe_2O_3 (MVS)	1.5	ba	60	86	400
11	b	Me	Et	a	Ph	Rh/PBI (MVS)	1.5	ba	51	89	340
12	b	Me	Et	a	Ph	Rh/ $\gamma\text{-Al}_2\text{O}_3$ (MVS)	1.5	ba	36	87	240
13	b	Me	Et	a	Ph	Rh/C (comm.)	1.5	ba	34	81	227
14	d	Me	<i>t</i> -Bu	a	Ph	Rh/C (MVS)	1.5	da	75	96	500
15	d	Me	<i>t</i> -Bu	a	Ph	Rh/C (MVS)	4	da	96	97	—
16	e	—	$(\text{CH}_2)_6$ —	a	Ph	Rh/C (MVS)	6	ea	100	96	—

^a Reaction conditions: 3 mmol of RMe_2SiH , 3 mmol of alkyne, 3×10^{-3} mmol of Rh, 3 mL of CH_2Cl_2 , 0.3 mmol of DBU, 100 °C, 30 atm CO; silylformylation by-products were detected by ¹H NMR spectroscopy.

^b Determined by GLC and ¹H NMR spectroscopic analysis of the reaction mixture after work up.

^c SA: $[\text{mmol}(\text{silane})/\text{mgat Rh} \cdot \text{time of reaction(h)}] \text{ conv.}\%$.



Scheme 5.

solution must be kept at $-40\text{ }^{\circ}\text{C}$ to avoid decomposition of the SMA and must be manipulated under argon.

Finally, even if *t*-BuMe₂SiH seems to favour the cyclisation process (Table 3, entries 1–3 vs. 4,5), the use of Me₂PhSiH is to be preferred in the synthesis of the β -lactones since in this case the silyl moiety can be easily removed by fluoride promoted rearrangements generating α -methylphenyl- β -lactones (Scheme 5) [38].

Unfortunately, the silylcarbo-cyclisation reactions performed with dimethylphenylsilane were characterised by a loss of chemoselectivity towards the β -lactone ring and relevant yield of the corresponding β -silylalkenals was observed (Table 3, entries 4 and 5). However, MVS Rh/C catalyst confirmed its better chemoselectivity and higher specific activity than the Rh₄(CO)₁₂ (Table 3, entry 4 vs. 5).

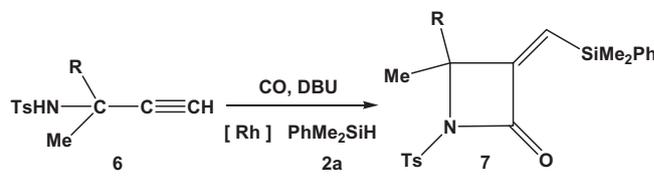
The steric requirements of the silylcarbo-cyclisation reactions were respected using 3-dialkylpropargyl alcohols **1b,d,e** as reported in entries 6–16 of Table 3. Initially, the rhodium catalysts were tested in the silylcarbo-cyclisation of 3-methyl-1-pentyn-3-ol **1b** that had already been successfully submitted to the silylformylation process in the presence of Me₂PhSiH (Table 2, entries 9 and 10). By comparing Rh/C (MVS) with Rh₄(CO)₁₂ (Table 3, entries 6 and 7) we could observe that quantitative conversion of the reagents was obtained after 4 h and that both catalysts yielded the expected β -lactones with high chemoselectivity (>90%).

Subsequently, in order to investigate the catalytic performances of the supported catalysts, the reactions were stopped after 1.5 h and the specific activity of the rhodium species was calculated. As it is evident from the data reported in Table 3 (entries 9–12), all the supported rhodium species prepared according to the MVS methodology displayed specific activities higher than Rh₄(CO)₁₂. The nature of the support plays a fundamental role on the catalytic behaviour: while Rh/C (MVS) was indubitably the best catalytic species, Rh/ γ -Al₂O₃ (MVS) promoted the cyclisation reaction more slowly, but resulted a better catalyst than the commercial Rh/C in terms of conversion and selectivity (Table 3, entries 9 and 12 vs. entry 13).

Particularly interesting resulted the catalytic efficiency showed by the rhodium nanoparticles deposited on the polymeric matrix PBI (Table 3, entry 11), a thermo-oxidatively stable material (up to 600 $^{\circ}\text{C}$) encouraging support for catalytic species [75]. Indeed, Rh/PBI showed an SA more than twice the specific activity of Rh₄(CO)₁₂.

The promising results of specific activity obtained for the MVS nanostructured catalysts can be reasonably related to the morphological properties of the metal nanoparticles obtained by means of this technique, i.e. very small mean diameter and narrow size distribution ($d_m \approx 1\text{--}2\text{ nm}$, Table 1, entries 3–6). Indeed, in the case of Rh/C purchased by Engelhardt and characterised by rhodium nanoparticles with a larger mean diameter and a wider size distribution (Table 1, entry 1 vs. 3) a dramatic reduction of catalytic activity in the silylcarbo-cyclisation reaction of 3-methyl-1-pentyn-3-ol **1b** was observed (less than an half than the corresponding MVS species), together with a remarkable loss of chemoselectivity towards the β -lactone product **4ba** (Table 3, entry 9 vs. 13).

The good catalytic efficiency of Rh/C (MVS) was confirmed by the results obtained in the synthesis of β -lactones **4da** and **4ea**



Scheme 6.

Table 4

Silylcarbo-cyclisation of *p*-toluenesulphonamides with Me₂PhSiH (**2a**).

Entry ^a	R	6	[Rh]	<i>t</i> (h)	7	Conv. (%) ^b	Sel. (%) ^b	SA ^c
1	Et	a	Rh ₄ (CO) ₁₂	4	aa	100	96	–
2	Et	a	Rh/C (MVS)	4	aa	98	90	–
3	Et	a	Rh/Fe ₂ O ₃ (MVS)	4	aa	96	86	–
4	Et	a	Rh/ γ -Al ₂ O ₃ (MVS)	4	aa	27	89	–
5	Et	a	Rh ₄ (CO) ₁₂	1.5	aa	28	81	47
6	Et	a	Rh/C (MVS)	1.5	aa	17	89	113
7	Et	a	Rh/Fe ₂ O ₃ (MVS)	1.5	aa	16	78	107
8	Et	a	Rh/ γ -Al ₂ O ₃ (MVS)	1.5	aa	12	92	80
9	Et	a	Rh/PBI (MVS)	1.5	aa	12	89	80
10	Et	a	Rh/C (comm.)	1.5	aa	6	95	40
11	Et	a	Rh/ γ -Al ₂ O ₃ (comm.)	1.5	aa	0	–	–
12	Me	b	Rh ₄ (CO) ₁₂	4	ba	94	94	–
13	Me	b	Rh/C (MVS)	4	ba	94	91	–
14	Me	b	Rh/C (MVS)	1.5	ba	32	99	213
15	Me	b	Rh/ γ -Al ₂ O ₃ (MVS)	4	ba	33	96	81
16	<i>t</i> -Bu	c	Rh ₄ (CO) ₁₂	4	ca	65	100	41
17	<i>t</i> -Bu	c	Rh/C (MVS)	4	ca	75	100	187

^a Reaction conditions: 3 mmol of Me₂PhSiH, 3 mmol of alkyne, 3×10^{-3} mmol of Rh, 3 mL of CH₂Cl₂, 0.3 mmol of DBU, 100 $^{\circ}\text{C}$, 30 atm CO; small amounts of (*Z*)- β -silylalkenals were detected by ¹H NMR spectroscopy.

^b Determined by GLC and ¹H NMR spectroscopic analysis of the reaction mixture after work up.

^c SA: [mmol(silane)/mgat Rh·time of reaction(h)] conv.%.

(Table 3, entries 14–16) from their precursors 3,4,4-trimethyl-1-pentyn-3-ol **1d** and 1-ethynylcyclohexanol **1e** which yielded the desired products almost quantitatively and with excellent chemoselectivity (>95%).

2.4. Silylcarbo-cyclisation of propargyl amides: synthesis of β -lactams

Prompted by the good results obtained in the synthesis of β -lactones, we tested our supported catalysts in the silylcarbo-cyclisation of *p*-toluenesulphonamides in order to prepare β -lactam rings. Initially *N*-(1-methyl-1-ethyl-2-propynyl)-*p*-toluenesulphonamide **6a** was chosen as model substrate and reacted with equimolar amount of Me₂PhSiH **2a**, 10 mol% of DBU, in the presence of 0.1 mol% of rhodium catalyst, under 30 atm of CO, at 100 $^{\circ}\text{C}$ for 4 h (Scheme 6, Table 4, entries 1–11).

Supported species Rh/C, Rh/Fe₂O₃ and Rh/ γ -Al₂O₃, prepared according to MVS technique, were able to promote the cyclisation reaction with almost total chemoselectivity towards the β -lactam **7aa** (Table 4, entries 2–4). The reaction rate resulted dependent on the nature of the support: after 4 h, Rh/ γ -Al₂O₃ afforded the β -lactam derivative with a conversion much lower than Rh/C and Rh/Fe₂O₃ which showed catalytic performances comparable to Rh₄(CO)₁₂, taken as homogeneous reference catalyst (Table 4, entry 1 vs. entries 2–4).

To get a deeper insight into the catalytic behaviour of the supported rhodium species, we compared the specific activity (SA) of the catalysts at low conversion of the reagents (i.e. after 1.5 h). Analogously to what observed in the silylcarbo-cyclisation of

propargyl alcohols **1b,d,e** (Table 3), it is clear from the data reported in Table 4 (entries 7–9) that all the MVS catalysts resulted more reactive than $\text{Rh}_4(\text{CO})_{12}$ and that MVS Rh/C appeared to be the best catalytic system (entry 6). Rhodium nanoparticles deposited on Fe_2O_3 and $\gamma\text{-Al}_2\text{O}_3$ and on the organic matrix PBI showed good specific activities too (Table 4, entries 7 and 9), thus confirming the importance of the catalyst morphology, i.e. small particles homogeneously dispersed on the support. Indeed, commercial Rh/C 5% characterised by larger rhodium clusters promoted the formation of **7aa** three times slower than the corresponding MVS species (Table 4, entry 6 vs.10) and commercial Rh/ $\gamma\text{-Al}_2\text{O}_3$ resulted totally inert (Table 4, entry 11).

The good efficiencies and chemoselectivities towards the synthesis of β -lactam ring showed by the MVS derived catalysts was confirmed by the reactions of Me_2PhSiH **2a** with alkynes **6b** and **6c** (Table 4, entries 13–17). Again, Rh/C resulted the best choice in terms of specific activity (entries 13 and 17) affording the desired β -lactams in high yields, regardless the structural features of the *p*-toluenesulphonamides.

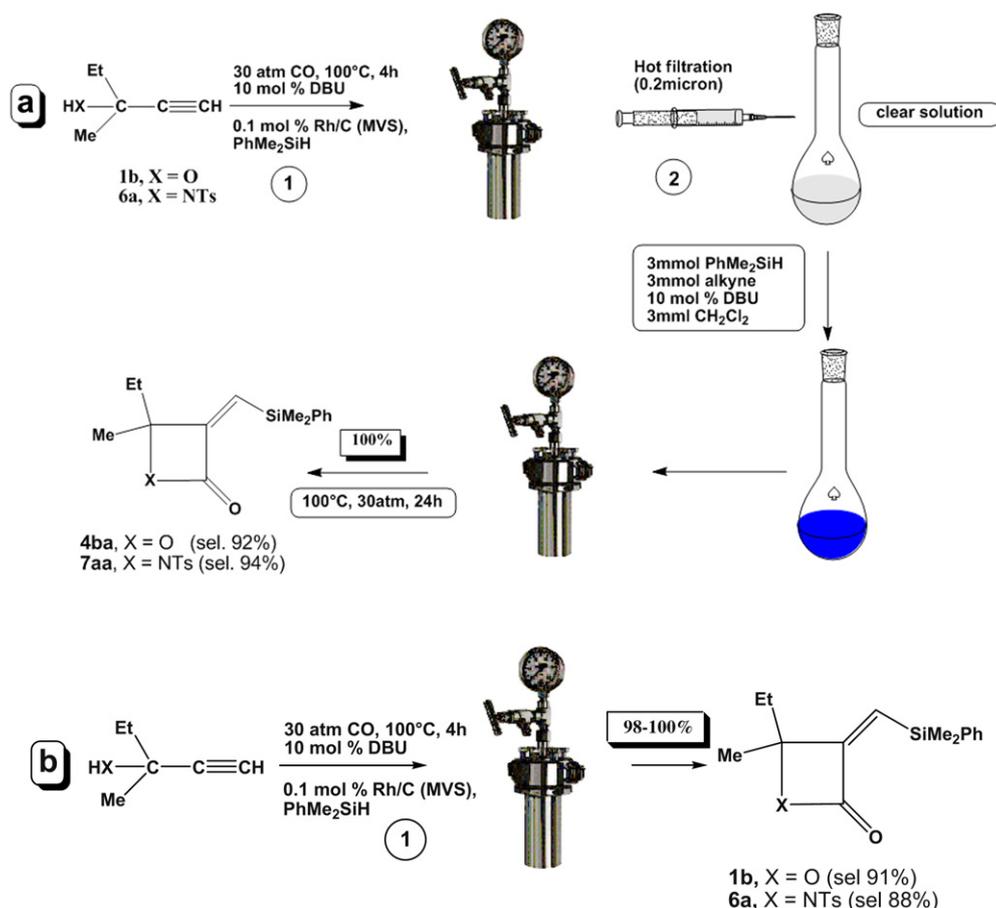
2.5. Preliminary investigation on the nature of the catalytically active species

To obtain more information on the characteristics of the real species catalytically active in the silylcarbocyclisation reactions, we performed two experiments reacting, respectively, 3-methyl-1-pentyn-3-ol **1b** and *N*-(1-methyl-1-ethyl-2-propynyl)-*p*-toluenesulphonamide **6a** under the usual experimental conditions (equimolar amount of Me_2PhSiH , 10 mol% of DBU, 100 °C, 30 atm of CO) in the

presence of 0.1 mol% of Rh/C (MVS). After 4 h, the CO pressure was discharged and the reaction mixture was filtered through a Teflon filter (0.2 μm) in order to remove all suspended metal and/or carbon particles. Then, the clear solutions obtained were added with fresh reagents (3 mmol of acetylenes, 3 mmol of Me_2PhSiH , 0.3 mmol of DBU and 3 mL of CH_2Cl_2) and reintroduced into autoclaves. The reaction mixtures were reacted for further 4 h at 100 °C under 30 atm of carbon monoxide (Scheme 7, path a). Contemporaneously, two blank experiments of silylcarbocyclisations of **1b** and **6a** were carried out under the usual experimental conditions affording the corresponding β -lactone and β -lactam in high yields and selectivity (Scheme 7, path b).

The obtained data are described in Fig. 3. The conversions of the alkyne derivatives (98–100%) **1b** and **6a** in the blank experiments are reported in columns 1 and 3, respectively, while columns 2 and 4 indicate the data obtained in the leaching tests.

In the leaching procedures (i.e. recharging tests), after usual work up, both chromatographic and spectroscopic analyses indicated a complete consumption of the reagents (100%) and a high selectivity towards the β -lactone **4ba** and the β -lactam **7aa**. Since all rhodium particles supported on carbon should have been removed from the crude products during the filtration step (Scheme 7, path a, step 2), the obtained results clearly indicate the presence of soluble catalytically active metal nanoparticles in the filtered solutions. We can conclude that the Rh/C (MVS) system behaves not as a heterogeneous catalyst but as a source of homogeneous rhodium nanoparticles that represent the real active species. The lower catalytic performances observed for the solvated rhodium atoms deposited on the metal oxides (Rh/ $\gamma\text{-Al}_2\text{O}_3$ and Rh/



Scheme 7.

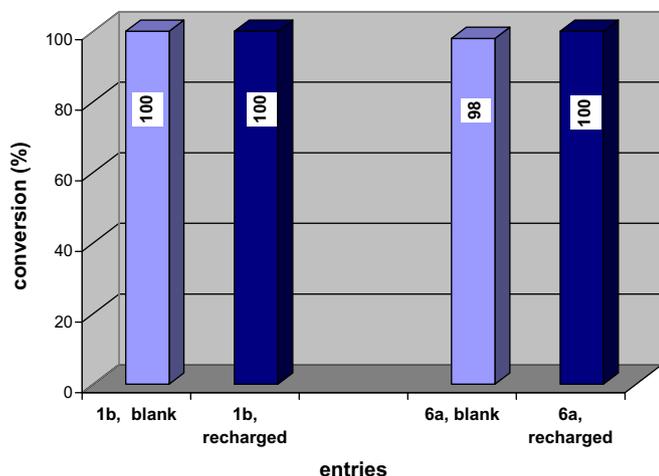


Fig. 3. Results of leaching tests.

Fe₂O₃) and on polybenzimidazole (Rh/PBI) could be related to a minor amount of rhodium leached from these matrices due to their stronger bonds with the metal particles. Moreover, while very small “naked” particles of rhodium are leached from the MVS catalysts, the larger dimensions of commercial rhodium deposited on carbon and alumina could account for the lower specific activities observed in these cases.

3. Conclusions

In this paper we have demonstrated that MVS derived rhodium nanoparticles supported on inorganic and organic matrices are able to promote silylcarbocyclisation reactions thus generating β -lactones and β -lactams in high yields. Among the prepared catalysts, MVS Rh/C resulted the best choice in terms of activity and selectivity. Besides, all the other MVS species showed a specific activity much better than the corresponding commercial catalysts Rh/C and Rh/ γ -Al₂O₃ and also than Rh₄(CO)₁₂ chosen as homogeneous reference species. The good efficiencies observed with the MVS catalysts seem to be related to their structural features, i.e. very small rhodium particles well dispersed on the support. The minor specific activity observed in the cases of metal particles deposited on polar matrices such as PBI and Fe₂O₃ could be due to stronger interactions between the rhodium nanoclusters and the support. As a matter of fact, preliminary experiments on Rh/C aimed to investigate the real nature of the catalytic species unfortunately showed a remarkable leaching of rhodium from carbon into solution. We can conclude that Rh/C, and reasonably all MVS supported catalysts, acts as a reservoir, stable with ageing at room temperature, of very active nanoparticles that are released from the support under the reaction conditions.

4. Experimental

4.1. General

All operations involving the MVS products were performed under a dry argon atmosphere. The co-condensation of rhodium and mesitylene was carried out in a static reactor previously described [73]. The “mesitylene-solvated Rh atoms” solution was worked up under argon atmosphere with the use of the standard Schlenk techniques. The amount of rhodium in the solutions was determined by atomic absorption spectrometry in an

electrochemically heated graphite furnace with a Perkin Elmer 4100ZL instrument. The limit of detection calculated for rhodium was 2 ppb.

Me₂PhSiH (**2a**), *t*-BuMe₂SiH (**2b**), 1-hexyne (**1a**) and propargyl alcohols **1b–e** were purchased by Sigma–Aldrich and distilled before use. *N*-propargyl-*p*-toluenesulphonamides **5a–c** were prepared as previously reported [50]. Solvents were purified by conventional methods, distilled and stored under argon.

Commercial γ -Al₂O₃ (Chimet product, type 49, surface area 110 m²/g, mean particle diameter 3.1 μ m), C (Chimet product, surface area 890 m² g⁻¹), Fe₂O₃ (Aldrich product, powder, 99.5%, 1.0 μ m average particle size, surface area 2.1 m² g⁻¹), were dried in a static oven before use. Polybenzimidazole (PBI) in beaded form (250–500 μ m, surface area 20 m² g⁻¹) was gently provided from Prof. B. Corain (University of Padova).

Commercial Rh/ γ -Al₂O₃ (5 wt.% of Rh, surface area 130 m²/g) and Rh/C (5 wt.% of Rh, surface area 900 m²/g) were Engelhardt products. Rh₄(CO)₁₂ was prepared as previously described [76].

The GLC analyses were performed on a Perkin–Elmer Auto System gas chromatograph, equipped with a flame ionization detector (FID), using a SiO₂ column (DB1, 30 m \times 0.52 mm, 5 μ m) and helium as carrier gas.

4.2. Preparation of rhodium catalysts

4.2.1. Synthesis of solvated Rh atoms

In a typical experiment, rhodium vapour, generated by resistive heating of a tungsten wire surface coated with electrodeposited rhodium (110 mg), was co-condensed at liquid nitrogen temperature with mesitylene (45 ml) in the glass reactor chamber of the MVS apparatus in ca. 45 min. The reactor chamber was warmed to the melting point of the solid matrix (ca. –30/–40 °C) and the resulting red-brown solution was siphoned at low temperature in a Schlenk tube and kept in a refrigerator at –20 °C. The content of the metal solution was 1 mg rhodium/ml (0.097 mg atom/ml).

4.2.2. Preparation of Rh/ γ -Al₂O₃ catalyst (1% w/w)

The Rh/mesitylene reaction solution (5 ml, 5 mg Rh) was added to a suspension of γ -Al₂O₃ (500 mg) in mesitylene (10 ml). The mixture was stirred for 24 h at room temperature. The colourless solution was removed and the light-brown solid, containing 1 wt.% Rh, was washed with *n*-pentane and dried under reduced pressure.

4.2.3. Preparation of Rh/C catalyst (1% w/w)

The Rh/mesitylene reaction solution (5 ml, 5 mg Rh) was added to a suspension of carbon (500 mg) in mesitylene (10 ml). The mixture was stirred for 24 h at room temperature. The colourless solution was removed and the light-brown solid, containing 1 wt.% Rh, was washed with *n*-pentane and dried under reduced pressure.

4.2.4. Preparation of Rh/Fe₂O₃ catalyst (0.98% w/w)

The Rh/mesitylene reaction solution (4.9 ml, 4.9 mg Rh) was added to a suspension of Fe₂O₃ (503 mg) in mesitylene (10 ml). The mixture was stirred for 5 days at room temperature. The colourless solution was removed and the solid, containing 0.98 wt.% Rh, was washed with *n*-pentane and dried under reduced pressure.

4.2.5. Preparation of Rh/PBI catalyst (0.98% w/w)

The Rh/mesitylene reaction solution (3.9 ml, 3.9 mg Rh) was added to a suspension of PBI (398 mg) in mesitylene (10 ml). The mixture was stirred for 5 days at room temperature then treated with hydrogen. The colourless solution was then removed and the solid, containing 0.98 wt.% Rh, was washed with *n*-pentane and dried under reduced pressure.

4.3. Characterization of the catalysts

High resolution transmission electron microscopy (HR-TEM) images of the materials (powder grains dispersed on lacey carbon Cu grids) were obtained using a JEOL 3010-UHR with an acceleration potential of 300 kV.

Histograms of the particle size distribution were obtained by considering at least 300 particles on the TEM images and the mean particle diameter (dm) was calculated as $dm = \sum d_i n_i / \sum n_i$, where n_i was the number of particles of diameter d_i .

4.4. Catalytic reactions

4.4.1. Silylformylation reactions

Silylformylation reactions were run in a 25 mL stainless steel autoclave fitted with a Teflon inner crucible and a stirring bar. In a typical run, equimolar amounts of Me_2PhSiH and 1-alkyne, toluene or CH_2Cl_2 (2–3 mL) and 0.1 mol% of rhodium catalyst were put under CO atmosphere in a Pyrex “Schlenk” tube. This solution was introduced into the previously evacuated (0.1 Torr) autoclave by a steel siphon. The reactor was pressurised with carbon monoxide and the mixture was stirred at the chosen temperature for a specified time. After removal of excess CO (fume hood), the reaction mixture was diluted with pentane or CH_2Cl_2 , filtered (Celite) and concentrated by bulb to bulb distillation (1 Torr). The residue was purified by column chromatography on silica gel affording the pure aldehydes [50,72].

4.4.2. Silylcarbocyclisation reactions

Catalytic runs were performed in a 25 mL stainless steel autoclave fitted with a Teflon inner crucible and a stirring bar. In a typical run, 3 mmol of alcohol or amide, 3 mL of a freshly distilled CH_2Cl_2 , 3 mmol of R_3SiH , 0.3 mmol of DBU were put, via syringe and under CO atmosphere, in a Pyrex Schlenk tube. This solution was introduced in the autoclave, previously placed under vacuum (0.1 mmHg) and charged with 0.1 mol% of rhodium catalyst, by a steel siphon. The reactor was pressurised to 30 atm of CO and stirred at 100 °C for the required times. The autoclave was then cooled to room temperature and the excess of CO was removed under fume hood. The reaction mixture was diluted with CH_2Cl_2 , filtered on silica gel and concentrated under reduced pressure. The reagents conversion and the products composition were determined by GLC and ^1H NMR. The purification of the crude oil by column chromatography on silica gel afforded the pure β -lactones [38] and β -lactams [50].

4.4.3. Leaching procedure

Leaching studies were performed using the hot filtration technique. After 4 h reaction of a standard catalytic run, the CO pressure was removed under fume hood, the reaction mixture was filtered at 100 °C through syringe fitted with a 0.2 μm Teflon filter, in order to remove all fine particles. Then 3 mmol of alcohol or amide, 3 mL of a freshly distilled solvent, 3 mmol of Me_2PhSiH , 0.3 mmol of DBU were added to the clear solution obtained which was introduced into an autoclave by a steel siphon and reacted under the standard reaction conditions for further 4 h. After the usual work up, the reagents conversion and the products composition were determined by GLC and ^1H NMR.

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