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# Enhanced PAHs adsorption using iron-modified coal-based activated carbon via microwave radiation

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1	Enhanced PAHs adsorption using iron-modified coal-based
2	activated carbon via microwave radiation
3	Xinyu Ge <sup>a</sup> , Zhansheng Wu <sup>a,b</sup> *, Zhilin Wu <sup>b</sup> , Yujun Yan <sup>a</sup> , Giancarlo Cravotto <sup>b</sup> , Bang-Ce
4	$\mathbf{Ye^{a}}$
5	<sup>a</sup> School of Chemistry and Chemical Engineering, Shihezi University, Shihezi 832003, P.R.
6	China
7	<sup>b</sup> Dipartimento di Scienza e Tecnologia del Farmaco, University of Turin, Torino 10125, Italy
8	Corresponding author: Zhansheng Wu, Shihezi University, Shihezi 832003, P.R. China.
9	Tel: 86993-2055015, Fax: 86993-2057270, E-mail address: wuzhans@126.com.
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#### 23 ABSTRACT

As an effective adsorbent, coal-based activated carbon (CAC) was modified with iron 24 through microwave radiation to adsorb polycyclic aromatic hydrocarbons (PAHs) from 25 aqueous solutions. The effects of iron nitrate concentration, microwave power, and 26 microwave radiation time on CAC were investigated. The optimum modification conditions 27 were as follows: iron nitrate concentration, 0.05 M; microwave power, 300 W; and 28 microwave radiation time, 5 min (designated as 0.05Fe-MCAC). CAC and 0.05Fe-MCAC 29 were characterized using scanning electron microscopy, nitrogen adsorption-desorption, 30 surface acidity and basicity tests, and Fourier transform infrared spectroscopy. The 31 adsorption capacities of PAHs were also determined. After modification the following 32 phenomena occurred: pore structures developed; BET surface area increased from 686.06 to 33 1079.67  $m^2/g$ ; the number of oxygen-containing groups decreased; and basicity was 34 enhanced. The PAHs adsorption capacity of 0.05Fe-MCAC was higher than that of CAC. 35 The altered texture and chemical properties of 0.05Fe-MCAC played an important role in 36 PAHs adsorption. The pseudo-second-order models of CAC and 0.05Fe-MCAC fitted well. 37 The PAHs adsorption of 0.05Fe-MCAC owned lower activation energy and greater stability 38 than that of CAC. Results indicated that iron-modified CAC via microwave radiation is a 39 promising and efficient adsorbent of PAHs from aqueous solutions. 40

41

42 Keywords Coal-based activated carbon · Microwave radiation · Iron modification · PAHs
43 adsorption

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# 45 **1. Introduction**

Polycyclic aromatic hydrocarbons (PAHs) commonly refer to a large class of dangerous 46 47 and harmful ecosystem pollutants. They are generated during the incomplete combustion of hydrocarbons and other organic compounds, such as coal, petroleum, and biomass [1, 2]. 48 49 PAHs can be transported in long distances in water but cannot be easily biodegraded because of their chemical persistence and semi-volatile nature [3]. In addition their toxic, mutagenic, 50 and carcinogenic properties, they are considered as priority pollutants [4]. PAHs are 51 effectively removed from aqueous solutions through adsorption [5, 6]. Nevertheless, 52 53 economical and applicable absorbents should be developed to remove PAHs efficiently.

Activated carbon (AC) is characterized by a wide surface area and developed porosity; 54 as such, it is considered a highly promising absorbent for a wide range of technical 55 56 applications [6–8]. AC is also a commonly used adsorbent in wastewater treatments worldwide. AC is modified to regulate its pore structure and chemical properties. This 57 process is an effective route to enhance the removal efficiency of AC as an adsorbent of 58 various pollutants. Liu et al. [9] modified bamboo-based AC and found that the modified AC 59 can effectively adsorb methylene blue. Shaarani et al. [10] demonstrated that 60 61 ammonia-modified AC for adsorption of 2, 4-dichlorophenol was superior to the AC. Yin et al. [11] also modified AC-enhanced contaminant uptake from aqueous solutions. However, 62 coal-based AC (CAC) has been rarely developed as an absorbent of PAHs from aqueous 63 solutions [12–14]. Other materials are also more commonly used than CAC. Organic 64 compound adsorption by AC is generally influenced by various properties, such as pore size, 65 pore diameter distribution, surface properties, and surface functional groups [15, 16]. 66

67 Therefore, structure and surface functional groups should be appropriately controlled to68 improve the adsorption of PAHs from aqueous solutions.

69 Metal-modified AC may provide an enhanced porosity structure and can vary in terms of pore structure and surface functional groups; thus, adsorption properties are altered [17]. 70 Various metal oxides, such as manganese, mercury, and iron, have been added to AC to 71 improve their adsorption performance [18–20]. However, iron-modified CAC used for the 72 adsorption of PAHs from aqueous solutions has yet to be reported. Microwave is currently 73 used in various fields to heat dielectric materials because this technique requires a 74 75 considerably short treatment time and consumes low energy. In our previous study, microwave radiation can change the physical properties of AC [14]. Thus, iron-modified 76 CAC via microwave radiation should be investigated to enhance the adsorption of PAHs. 77

78 This study aimed to modify CAC with iron via microwave radiation and to investigate the properties of the modified CAC and its adsorption capacities for PAHs from aqueous 79 solutions. CAC and 0.05Fe-MCAC were characterized through scanning electron 80 81 microscopy (SEM), nitrogen adsorption-desorption, surface acidity and basicity, and Fourier transform infrared spectroscopy (FTIR) methods. The adsorption capacity of naphthalene on 82 0.05Fe-MCAC was also examined, and the adsorption kinetics of PAHs on CAC and 83 0.05Fe-MCAC were systematically analyzed. PAHs adsorption on CAC and 0.05Fe-MCAC 84 were compared, and the correlation of this property with their structures was determined. 85 This work could evaluate the effectiveness of 0.05Fe-MCAC in the removal of PAHs from 86 87 aqueous solutions and could enhance our understanding of the adsorption behavior of PAHs onto 0.05Fe-MCAC. 88

# 89 2. Materials and methods

## 90 2.1. Preparation of CAC

91 Coal-based activated carbon (CAC) was prepared according to our previous study [21], where the used coal (Xinjiang Tebian Electric Apparatus Stock Co., Ltd, China) was 92 93 activated using potassium hydroxide under microwave radiation. Microwave radiation was 94 conducted in a 2.45 GHz microwave oven (MM823LA6-NS, Midea). The preparation conditions of CAC were as follows: hydroxide potassium-to-coal ratio (w/w), 1:1; 95 microwave power, 700 W; and radiation time, 10 min. The obtained products were in an 96 97 air-dried oven at 110 °C for 4 h and marked as CAC. All of the chemicals and reagents used in this study were of analytical grade. 98

# 99 2.2. Modification of iron nitrate via microwave radiation

In this study, 0.2 g of CAC absorbent was added to a 150 mL conical flask with 15 mL of different concentrations (0.05-1 M) of Fe(NO<sub>3</sub>)<sub>3</sub> solution, and ultrasound was conducted for 2 h. The mixture was heated in a microwave oven (MCR-3, Shanghai Keli) at microwave power of 100–700 W and microwave radiation times of 1–8 min. After modification treatment, the mixture was filtered and extensively washed with double distilled water and dried in an oven at 110 °C for 4 h. These samples were named as Fe-MCAC and 0.05 M of Fe(NO<sub>3</sub>)<sub>3</sub>-modified sample was designated as 0.05 Fe-MCAC.

- 107 2.3. Characterization of CAC and 0.05Fe-MCAC
- 108 2.3.1. SEM

109 The morphologies of carbon samples were observed on scanning electron microscopy
110 (SEM, JEOL, JSM-6490LV, Japan) with an acceleration voltage of 15 kV. Prior to analysis,

- 111 the samples were dried at 383 K and stored in a desiccator overnight.
- 112 2.3.2. Fourier transform infrared (FTIR) spectrometer
- For FTIR measurements, the CAC and 0.05Fe-MCAC samples were blended with KBr to form pellets; the spectra were obtained on a PHI5700 ESCA spectrophotometer in the range of 4000-400 cm<sup>-1</sup> at 4 cm<sup>-1</sup> resolution.
- 116 2.3.3. BET surface area and pore structure analysis
- The Brunauer-Emmett-Teller (BET) surface area and porous properties of the CAC and
  0.05Fe-MCAC samples were determined from the N<sub>2</sub> adsorption at 77 K using a surface
  area analyzer (SI/MP, Quantachrome, USA).
- 120 2.3.4. Surface acidity and basicity
- The amphoteric characteristics of the CAC and 0.05Fe-MCAC samples were characterized by measuring the amount of the surface functional groups using the acid-base titration method proposed by Boehm [22]. According to this method and our reported studies [14, 22], 200 mg of each sample was added to 25 mL solutions of 0.05 M: sodium hydroxide, sodium carbonate, sodium bicarbonate and hydrochloric acid, respectively. The mixture was oscillated for 24 h in constant temperature vibrator at 25 °C, and the resulting suspensions were filtered for estimating the residual base/acid.
- 128 2.4. Adsorption test
- 129 2.4.1. Adsorption of PAHs from aqueous solution

Naphthalene, phenanthrene, pyrene were selected as the typical compounds, which are
commonly exist in wastewater/soil mediums. 15 mg of the carbon samples were added into
flask containing 100 mL, 30.0 mg/L of naphthalene, phenanthrene, and pyrene solution at

20 °C, respectively. After agitation for 60 min, the mixture solution was filtered, and
naphthalene, phenanthrene, and pyrene concentrations were measured using a UV-75N
spectrophotometer at 218 nm, 248 nm and 237 nm, respectively. The amounts of naphthalene,
phenanthrene, and pyrene on samples were calculated using the average of the three data.

137 2.4.2. Adsorption kinetic

Naphthalene, phenanthrene, and pyrene adsorption kinetics were evaluated at 10, 20, 30, and 40 °C, respectively. The initial concentration was set as 30 mg/L, and the samples were reacted at different contacting time intervals. The mixture was separated through filtration. Naphthalene, phenanthrene, and pyrene concentrations were determined using a UV-75N spectrophotometer. The amounts of naphthalene, phenanthrene, and pyrene at time t (min),  $q_t$ (mg/g), can be calculated according to Eq. (1),

144 
$$q_{t} = \frac{(C_{0} - C_{t}) \times V}{m}$$
 (1)

where  $C_t$  (mg/L) is the liquid-phase concentration of naphthalene, phenanthrene, and pyrene at any time t, respectively.

147 2.5. Regeneration of spent carbon

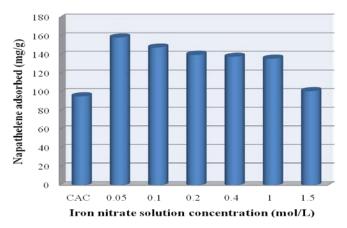
The 0.05Fe-MCAC adsorbed pyrene sample was desorbed and immersed in 100 mL absolute ethanol for 90 min. The carbon sample was removed and dried in vacuum at 110 °C for 24 h. The regeneration of carbon was determined, and the pyrene adsorption capacity was calculated repeatedly by using the described adsorption method. Desorption experiments were conducted again using the same adsorption method, and the cycle was repeated thrice.

# 153 **3. Results and discussion**

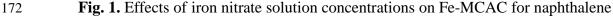
154 3.1. Adsorption capacity of Fe-MCAC for naphthalene

#### 155 *3.1.1. Effects of iron nitrate solution concentrations*

We investigated the effects of the concentration of iron nitrate solution on the 156 preparation of Fe-MCAC for naphthalene adsorption under the same microwave radiation 157 conditions (Fig. 1). As the concentration of iron nitrate solution increased, the amount of 158 naphthalene adsorbed on Fe-MCAC gradually decreased. The 0.05Fe-MCAC sample 159 modified with 0.05 M iron nitrate solution yielded a maximum adsorption capacity of 159.00 160 mg/g, which was significantly higher than the adsorption capacity of the CAC sample (95.74 161 mg/g). The Fe<sup>3+</sup> modification influenced the adsorption capacity of the adsorbent possibly 162 163 because of the change in texture and chemical properties on the surface of the CAC sample. Iron modification could enrich the pore structure of the Fe-MCAC sample, which enhanced 164 the adsorption capacity of Fe-MCAC for naphthalene [17]. However, a high iron nitrate 165 166 concentration was disadvantageous for the modified CAC for naphthalene adsorption in this study because excessive amounts of iron could be blocked pore of Fe-MCAC; as a 167 consequence, a small pore volume is obtained, and the adsorption efficiency is decreased 168 [20]. Considering that low concentration can save resources and enhance adsorption capacity, 169 we selected 0.05 M iron nitrate solution as the suitable modification concentration. 170



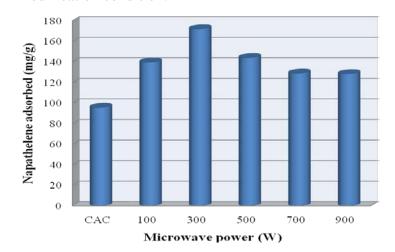
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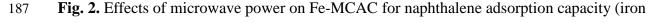
adsorption capacity (microwave power: 300 W, microwave radiation time: 5 min)

#### 174 *3.1.2. Effects of microwave power*

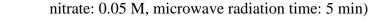
The effects of microwave power on the Fe-MCAC samples are presented in Fig. 2. The 175 176 increased amounts of naphthalene adsorbed on the Fe-MCAC sample were higher than those on the CAC sample. As radiation power was enhanced to 300 W, the amounts of naphthalene 177 178 on the Fe-MCAC sample were maximized possibly because the pore structure on the surface of the Fe-MCAC sample was greatly developed at a radiation power of up to 300 W. 179 However, the adsorption capacity decreased from 172.18 mg/g to 128.48 mg/g as power was 180 increased from 300 W to 900 W. This result was due to the fierce reaction at high microwave 181 182 power that reduces the surface area and porosity of the Fe-MCAC sample; as a consequence, the adsorption capacities of naphthalene were progressively decreased [23]. Hence, high 183 microwave power is disadvantageous for the modified CAC. A microwave power of 300 W 184 185 was the optimum modification condition.



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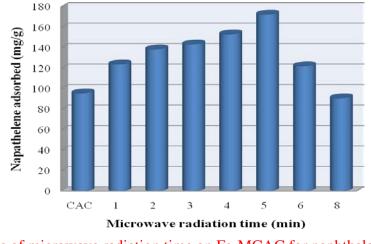


188



189 *3.1.3. Effects of microwave radiation time* 

190 The effect of microwave time on the preparation of Fe-MCAC can be observed by 191 increasing radiation time from 1 min to 5 min, which showed an enhancement of naphthalene capacity from 124.03 mg/g to 172.80 mg/g. Beyond the value of 5 min, the modified CAC obtained a lower naphthalene capacity (Fig. 3). A prominent drop was observed at 6 min probably as a result of a longer radiation time effect, which largely destroyed the pore walls between adjacent pores [24]. The results present that 5 min is the suitable period of time for modification because it provided the maximum naphthalene capacity with a value of 172.80 mg/g.



198

Fig. 3. Effects of microwave radiation time on Fe-MCAC for naphthalene adsorption
capacity (iron nitrate: 0.05M, microwave power: 300W)

From the discussion above, both iron nitrate solution concentration and microwave power had significant effects on the modified CAC for adsorption of naphthalene. The optimum conditions obtained were as follows: iron nitrate solution concentration 0.05 M, microwave power 300 W, and microwave time 5 min.

205 3.2. Characterization

206 *3.2.1. SEM* 

The morphologies of the CAC and 0.05Fe-MCAC samples were carried out by SEM. The pore size distribution of the CAC sample with high magnifying power (×1000) is uneven and exhibits less pores (Fig. 4). After iron modification treatment under microwave 210 irradiation, the surface of the 0.05Fe-MCAC sample was more porous than that of CAC (Fig. 4). Iron ion has high activity and easily enters the pore of 0.05Fe-MCAC. Several studies 211 also showed that microwave radiation treatment effectively developed pores on the surface 212 of the CAC and AC, which greatly enlarged the surface area and porous structure of the 213 214 carbons [14, 25]. Therefore, the developed porous structure could benefit the adsorption of 215 PAHs from aqueous solutions. In addition, 0.05Fe-MCAC can provide a large surface area for iron loading; and iron surface has stronger activity and can better combine with the 216 adsorbate, which may promote 0.05Fe-MCAC adsorption [14, 26]. Chen et al. showed that 217 218 iron-impregnated AC was highly effective in arsenic removal [20]. Considering these factors, the regulation of the pore structure of CAC and Fe<sup>3+</sup> loading are great of significance for 219 PAHs adsorption. 220

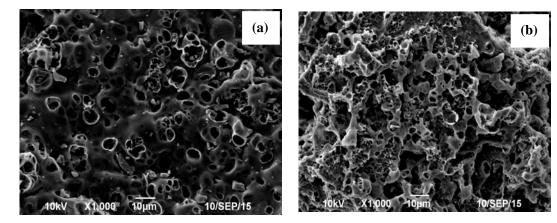
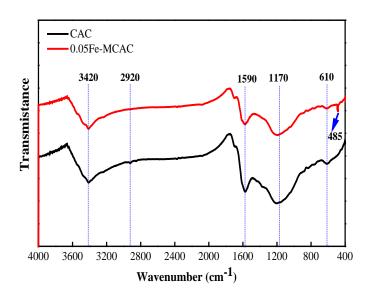


Fig. 4. Scanning electron microscope (SEM) micrograph: CAC (a); and 0.05Fe-MCAC (b) *3.2.2. Fourier transform infrared (FTIR) spectrometer*

FTIR analysis permitted the spectrophotometric observation of the adsorbent surface in the range of 400–4000  $cm^{-1}$  and served as a direct means for identifying the organic functional groups on the surface (Fig. 5). Insignificant changes, such as broadening of some bands and spectral shifts, were observed in the FTIR spectrum of the 0.05Fe-MCAC

compared with the FTIR spectrum of the CAC. The FTIR spectra of the CAC and 227 0.05Fe-MCAC presented a characteristic band at 3420 cm<sup>-1</sup>, which could be attributed to the 228 -OH stretching vibration [17, 20]. The band at approximately 2920 cm<sup>-1</sup> resulted from the 229 symmetric and asymmetric C–H stretching vibrations [25]. The difference in the intensity of 230 the 1590  $\text{cm}^{-1}$  between the two samples indicated that the modification process caused C=O 231 groups to decrease [25]. The peaks at approximately  $1170 \text{ cm}^{-1}$  represented the C–O 232 vibrations of various oxygen-containing groups. After iron modification, 233 the oxygen-containing functional group had a certain decrease. The most interesting changes in 234 the corresponding band were found at 485 cm<sup>-1</sup>, which could be attributed to the O-Fe 235 vibration. Rivera-Utrilla et al. also found this special band. This finding suggested that a 236 certain quantity of iron was loaded on the 0.05Fe-MCAC [27]. 237



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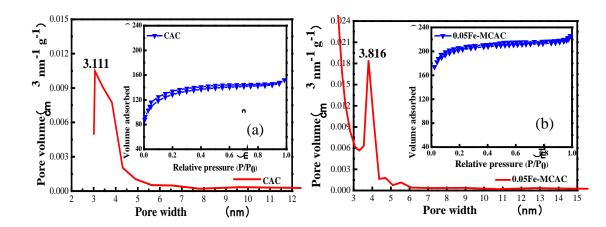
**Fig. 5.** FTIR analysis of the CAC and 0.05Fe-MCAC samples



241 The isotherms of the adsorption–desorption of  $N_2$  at 77 K were determined, as shown in

Fig. 6, to investigate the influence on the textural properties of the surfaces of the CAC and

0.05Fe-MCAC samples. According to IUPAC classification, the N<sub>2</sub> adsorption isotherms of 243 the CAC and 0.05Fe-MCAC samples were of type IV with a type-H<sub>4</sub> hysteresis loop. This 244 245 phenomenon has been reported in the scientific literature [14, 22]. These findings revealed a high portion of pores with indefinite pore size and shape in the 0.05Fe-MCAC particles [28]. 246 The saturated adsorption amount of  $N_2$  was as follows: 0.05Fe-MCAC > CAC. Hence, the 247 fixing of iron to 0.05Fe-MCAC modified its textural characteristics. From the pore size 248 analysis (Fig. 6), the two samples were essentially mesoporous because a vast majority of the 249 pores ranged between 2 and 10 nm. After iron modification, the average pore size of the 250 251 0.05Fe-MCAC sample was higher at 3.816 nm than that of the CAC (Fig. 6b). Thus, a large 0.05Fe-MCAC size would be conducive to PAHs adsorption. 252





253

Fig. 6. Pore size distributions of CAC (a); and 0.05Fe-MCAC (b)

The pore characteristics of the CAC and 0.05Fe-MCAC samples based on the  $N_2$ adsorption–desorption isotherms are shown in Table 1. The BET surface area, mesopore surface area, external specific surface area, total pore volume, and mesoporous pore volume increased after modification with iron nitrate solution, which could enhance the adsorption efficiency for PAHs adsorption. Moreno-Piraján et al. [17] found that the AC from bamboo waste modified with iron increased the BET surface area from 985.00 to 1357.00 m<sup>2</sup>/g

enhanced the adsorption for arsenite and arsenate. Ponvel et al. [28] showed that the metal 261 ion modification of AC developed pore properties, and the removal of 2, 4-dichlorophenol 262 from aqueous solutions became more effective. Therefore, the loading of iron via microwave 263 consequently radiation could enlarge pores and form mesopores [29]. 264 We accordingly speculated that the formed mesopores and developed pore properties could 265 benefit PAHs adsorption. 266

#### 267 **Table 1**

#### 268 BET analysis for CAC and 0.05Fe-MCAC

Physical parameters	CAC	0.05Fe-MCAC
BET specific surface area $(m^2/g)$	686.06	1079.67
Lamgmuir surface area (m <sup>2</sup> /g)	1042.56	1689.73
Mesopore surface area $(m^2/g)$	290.63	491.38
Total pore volume (cm <sup>3</sup> /g)	0.39	0.64
Mesoporous pore volume (cm <sup>3</sup> /g)	0.22	0.48

269 3.2.4 Surface acidity and basicity of CAC and 0.05Fe-MCAC

The total acidity and basicity of the CAC and 0.05Fe-MCAC samples are summarized 270 in Table 2. The Fe-MCAC sample was more basic than those on its surface. 271 One likely reason was that Fe<sup>3+</sup> was loaded onto the surface of 0.05Fe-MCAC, and oxygen 272 was removed; thus, the basicity properties were enhanced. The study by Rivera-Utrilla et al. 273 [27] showed that the increase in the basicity of AC surface favored the adsorption of organic 274 compounds. Strong basic properties of the 0.05Fe-MCAC sample were generally conducive 275 276 to PAHs adsorption from aqueous solutions. The amount of iron loading on the 0.05Fe-MCAC sample was 0.135 mmol/g (Table 2), which could be attributed to the changes 277 in the surface chemistry properties and increased the pore structure of the 0.05Fe-MCAC 278

sample [17]. Consequently, the loading of  $Fe^{3+}$  ions on the CAC surface increased the adsorption capacity for PAHs.

281 Table 2

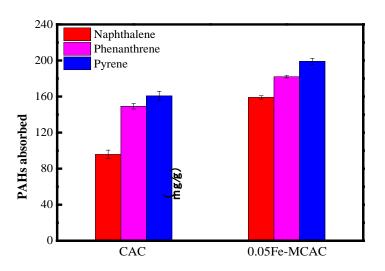
282 Total acidic and total basicity of CAC and 0.05Fe-MCAC

Total acidity (mmol/g)	Total basicity	Fe loading
	(mmol/g)	(mmol/g)
1.19	0.14	—
0.54	3.59	0.135
	1.19	1.19 0.14

283 3.3. Adsorption of PAHs on CAC and 0.05Fe-MCAC

Fig. 7 shows that the CAC and 0.05Fe-MCAC samples for the adsorption of 284 naphthalene, phenanthrene, and pyrene solutions at 20 °C had a similar result. After 285 286 modification was performed, the 0.05Fe-MCAC sample yielded a higher adsorption capacity for naphthalene, phenanthrene, and pyrene solutions than the CAC sample. The enhanced 287 adsorption capacity on the 0.05Fe-MCAC sample for naphthalene adsorption was the most 288 evident; in this finding, the adsorption capacity increased by 66.07% (Fig. 7). In the same 289 adsorption condition, the total adsorption capacity for PAHs on CAC and 0.05Fe-MCAC 290 pyrene > phenanthrene > samples followed this order: naphthalene. Using 291 292 petroleum-coke-derived porous carbon adsorption of PAHs from aqueous solutions, Yuan et al. [3] found that the adsorption capacity followed the same order in terms of adsorption 293 capacity. A similar behavior was reported for the CAC adsorption for naphthalene, 294 phenanthrene, and pyrene by Xiao et al [29]. Therefore, increasing the number of aromatic 295 296 rings (or  $\pi$ -electrons) in the PAH compound could increase the adsorption capacity for PAHs from aqueous solutions. This phenomenon could be attributed to the fact that molecules with 297 more aromatic rings show significantly higher adsorptive affinity than the aromatics with 298

less rings [30]. Moreover, PAHs and benzene molecules can form  $\pi$ - $\pi$  complex between the 299  $\pi$ -electrons of benzene rings and active sites on an AC surface [25, 29, 30]. In addition, the 300 affinity of 0.05Fe-MCAC to PAHs solution was greater than that of the other samples 301 because of iron modification. However, given that the high-activity iron-modified CAC via 302 microwave radiation provided the 0.05Fe-MCAC sample with a developed pore structure 303 and an enlarged pore size, we concluded that small-molecule PAHs could be easily adsorbed. 304 Thus, the 0.05Fe-MCAC sample had higher adsorption capacity of PAHs from aqueous 305 solutions. Compared with the CAC, the 0.05Fe-MCAC sample is a promising adsorbent for 306 307 PAHs from aqueous solution.



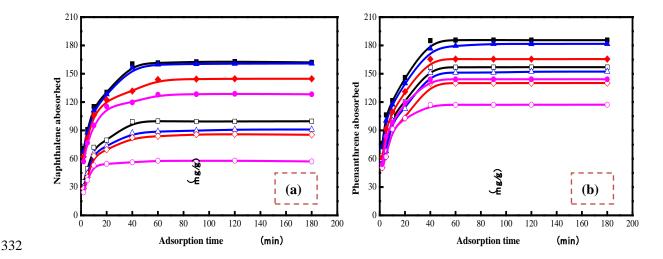
308 309



310 *3.4. Adsorption kinetics* 

The adsorption mechanism (adsorbed physically, e.g., by a dispersive force) associated with the removal of PAHs on the surfaces of the CAC and 0.05Fe-MCAC samples was explained [31]. The adsorption kinetics results showed that the increase in temperature reduced the adsorption capacity of naphthalene, phenanthrene, and pyrene adsorbed onto CAC and 0.05Fe-MCAC (Figs. 8a-c). This result indicated that low temperature favored the 316 adsorption of naphthalene, phenanthrene, and pyrene from aqueous solutions.

Fig. 8 shows that the adsorption of all PAHs appeared to have similar kinetic behavior 317 from 10 °C to 40 °C. Adsorption involves two distinguished periods, namely, an initial 318 period of rapid adsorption and a period of slow adsorption [14, 32]. The initial adsorption 319 320 stage was short in the first 10 min; a gradual process occurred until equilibrium was attained after a 40 min contact time; this finding indicated that the maximum sorption of naphthalene, 321 phenanthrene, and pyrene occurred for approximately 40 min (Fig. 8). The 0.05Fe-MCAC 322 sample adsorbed naphthalene, phenanthrene, and pyrene solutions to a greater extent than the 323 324 CAC sample. The adsorption process of PAHs on the 0.05Fe-MCAC sample was faster than that on other materials [12, 33]. A 2 mg modified periodic mesoporous organosilica (PMO) 325 reached adsorption equilibrium for the adsorption of PAHs aqueous solutions (8 mg/L, 5 mL) 326 327 for 24 h [12]. Using 0.5 g of an immature coal (leonardite) removed 100 µg/L of PAHs from aqueous solutions, and equilibrium time was reached at 24 h [33]. Moreover, the economical 328 dosage of absorbents is a symbol to evaluate the adsorption efficiency. The dosage of the 329 0.05Fe-MCAC sample was 15 mg in our study, which showed higher adsorption capacity 330 and faster adsorption than those in previous studies [12, 33]. 331



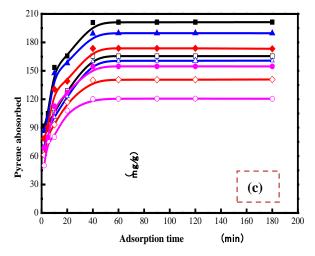


Fig. 8. Naphthalene (a), phenanthrene (b), and pyrene (c) on the CAC and 0.05Fe-MCAC
 kinetic curves at different temperature

336 (Conditions: Vacant points: CAC, Filled points: 0.05Fe-MCAC;  $\square / \square 10 \degree C$ ,  $\land / \land 20 \degree C$ ,

337 ◆/◊30 °C, ●/ ○ 40 °C)

In order to evaluate the adsorption kinetics of naphthalene, phenanthrene, and pyrene on the CAC and 0.05Fe-MCAC samples, the pseudo first order and the pseudo second order kinetic models were applied to the experimental data.

#### 341 *3.4.1. Pseudo-first-order kinetics*

333

# 342 The pseudo-first-order kinetic rate equation is expressed as:

343 
$$\frac{1}{q_t} = \frac{1}{q_e} + \frac{k_1}{q_e t}$$
 (2)

where  $k_1$  is the rate constant of pseudo-first-order sorption (min). The first-order rate constant can be determined from the slope of the linearized pseudo-first-order rate equation.

Table 3 shows the quantity of naphthalene, phenanthrene, and pyrene adsorbed at equilibrium for each of the CAC and 0.05Fe-MCAC samples synthesized using the pseudo-first-order model, constant kinetics, and a factor of correlation  $R^2$  between 0.8870–0.9860. These values suggest the dispersion of the experimental data and show that the adsorption of naphthalene, phenanthrene, and pyrene on the CAC and
0.05Fe-MCAC samples are not a first-order reaction.

#### 353 3.4.2. Pseudo-second-order kinetics

354 The pseudo-second-order kinetic rate equation is expressed as:

355 
$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e}$$
(3)

where  $k_2$  is the rate constant of pseudo-second-order sorption [g/(mg·min)]. The second-order rate constant can be determined from the intercept of the linearized pseudo-second-order rate equation.

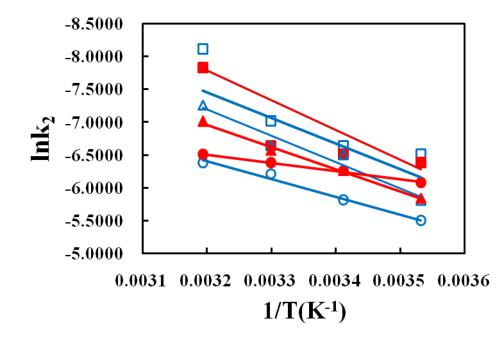
The amounts of naphthalene, phenanthrene, and pyrene adsorbed in equilibrium at 359 different temperatures, the velocity constant of the model, and the correlation factors were 360 obtained from the linearization of the model (Table 3). The pseudo-second-order model from 361 362 10 °C to 40 °C all had good fit for the CAC and 0.05Fe-MCAC samples with high correlation coefficients ( $R^2 = 0.9992 - 0.9997$ ). The  $q_{exp}$  values in the pseudo-second-order 363 model were closer to the experimental  $q_{cal}$  values than the values in the pseudo-first-order 364 365 model. This indicated the applicability of the second-order kinetic model to describe the adsorption processes of naphthalene, phenanthrene, and pyrene on the CAC and 366 0.05Fe-MCAC samples. This result also suggested that the adsorption process involved 367 368 chemical adsorption [14, 20]. We found that the 0.05Fe-MCAC sample had the best adsorption efficiency for naphthalene adsorption. From the literature, the adsorption of 369 naphthalene on naturally and chemically modified bentonites [1] and the adsorption of PAHs 370 on the CAC and modified CAC [14, 24] were best represented by the pseudo-second-order 371 model. 372

In engineering practice, the activation energy,  $E_a(kJ/mol)$ , is obtained from an Arrhenius equation (4):

376 
$$\ln k_2 = \ln A - \frac{E_a}{R} (\frac{1}{T})$$
 (4)

377 Where  $k_2$  is the rate constant of second-order adsorption, *A* is the frequency factor or the 378 Arrhenius constant, *R* is the universal gas constant (8.314 J/K mol) and *T* is the absolute 379 temperature (K).

When  $\ln k_2$  is plotted against the reciprocal of the temperature (1/*T*) as in Fig. 9, E<sub>a</sub> represents the slope shown in Table 3. We found that the modified sample had low activation energy for PAH adsorption, which may have improved the adsorption of PAH. Iron had a certain catalytic effect and enhanced the reaction rate. These low activation energy values of  $E_a$  ( $\leq$  40 kJ/mol) for adsorption of PAHs on the carbon adsorbents were mainly mechanisms of physical adsorption [34].



386

**Fig. 9.** Plots of  $\ln k_2/T^{-1}$  for adsorption of naphthalene, phenanthrene and pyrene on CAC and

388 0.05Fe-MCAC at different temperatures (Vacant points: CAC, Filled points: 0.05Fe-MCAC,

389

• / ● naphthalene, ▲ / ▲ phenanthrene, □ / ■ pyrene)

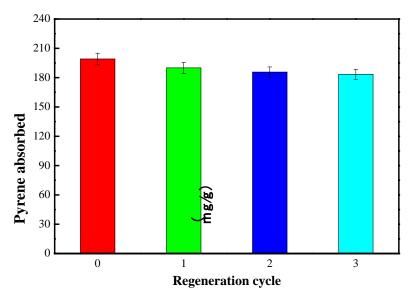
390	Table 3 Kinetic models parameters	for the adsorption of naphthalene, phenanthrene and
-----	-----------------------------------	---

391 pyrene on CAC and 0.05Fe-MCAC

				Pseudo-first-order		Pseudo-second-order				
Adsorbates	Samples	<i>Т</i> (°С)	$q_{ m exp}$ (mg/g)	qe (mg∕g)	$k_1$ (min <sup>-1</sup> )	$R^2$	q <sub>e</sub> (mg/g)	$k_2$ (g/(mg·mi n)	$R^2$	Ea (kJ/mol)
		10	105.00	99.65	3.70	0.9660	109.11	0.0041	0.9997	22.36
		20	95.74	83.45	4.60	0.9790	95.98	0.0030	0.9992	
	CAC	30	85.94	79.91	4.45	0.9710	90.91	0.0020	0.9998	
NT 1/1 1		40	57.94	52.50	3.00	0.9840	58.82	0.0017	0.9994	
Naphthalene	0.05Fe-MCAC	10	167.98	152.67	3.01	0.9490	169.04	0.0023	0.9993	
		20	159.00	146.67	3.00	0.9490	162.67	0.0019	0.9995	10.23
		30	144.68	132.86	2.71	0.9660	147.67	0.0017	0.9991	
		40	128.74	121.62	2.86	0.9750	132.86	0.0015	0.9995	
	CAC	10	160.96	142.86	2.71	0.8870	156.98	0.0030	0.9996	33.18
		20	149.20	130.86	3.40	0.9530	150.67	0.0015	0.9993	
		30	140.85	120.67	3.50	0.9770	144.32	0.0013	0.9995	
Phenanthrene		40	117.20	110.43	3.00	0.9350	123.00	0.0007	0.9994	
Phenanunrene	0.05Fe-MCAC	10	190.43	157.78	3.14	0.8730	185.58	0.0029	0.9998	
		20	181.99	173.47	3.71	0.9010	185.46	0.0019	0.9998	28.11
		30	165.52	142.86	2.71	0.9450	166.67	0.0014	0.9992	
		40	144.18	126.67	3.83	0.9860	146.73	0.0009	0.9993	
	CAC	10	172.46	165.67	2.50	0.8970	169.50	0.0015	0.9993	
		20	160.72	154.65	2.83	0.9020	163.32	0.0013	0.9994	38.75
		30	140.85	132.86	2.71	0.9450	146.67	0.0009	0.9993	
Demen		40	120.60	115.94	3.00	0.9860	124.00	0.0003	0.9992	
Pyrene	0.05Fe-MCAC	10	201.32	193.45	2.60	0.8900	206.13	0.0017	0.9995	
		20	199.07	189.98	2.61	0.8990	200.32	0.0015	0.9996	33 56
		30	173.25	163.94	3.00	0.8930	176.53	0.0013	0.9994	
		40	154.70	142.47	2.43	0.8980	156.32	0.0004	0.9993	

# 392 3.5 Regeneration of 0.05Fe-MCAC

The results of regeneration studies are presented in Fig. 10. The 0.05Fe-MCAC sample still had a high adsorption capacity for pyrene, which reached a level of 92.14% (183.43 mg/g) of the initial value after three cycles. This indicated that the modified sample had good stability, reusability, and adsorption effect for pyrene from aqueous solutions because the iron ion could exist in the surface structure of modified CAC in a stable form. The study reported by Shi et al. showed that naphthalene adsorption onto stable high-surface-area carbon still had high capacity after three cycles of alcohol treatment for the regeneration of the spent carbon [35].





**Fig.10.** Adsorption capacities of pyrene onto 0.05Fe-MCAC for three cycles

## 403 **4. Conclusions**

CAC was modified with iron via microwave radiation. The obtained 0.05Fe-MCAC 404 sample was characterized through SEM, FTIR, surface acidity and basicity, and nitrogen 405 adsorption-desorption methods. The surface chemistry and textural properties of CAC 406 407 changed when it was modified by iron nitrate via microwave radiation. The developed pore 408 structure, increased surface area, improved basic properties, and reduced oxygen-containing groups favored PAHs adsorption from aqueous solutions. The modified sample 409 (0.05Fe-MCAC) yielded a high adsorption capacity of 160.88 mg/g for naphthalene, 181.99 410 mg/g for phenanthrene, and 199.07 mg/g for pyrene. Among our observations, the increase 411

in the adsorption capacity of naphthalene on the 0.05Fe-MCAC sample was the most evident. 412 The modified sample was greater extent and more rapid for adsorbing naphthalene with less 413 414 aromatic rings than the CAC. Kinetic studies exhibited a faster adsorption rate of PAHs on the 0.05Fe-MCAC sample than the CAC. The pseudo-second-order model fitted well for 415 CAC and 0.05Fe-MCAC samples. Low temperature is favorable for the adsorption of 416 naphthalene, phenanthrene, and pyrene from aqueous solutions. The modified 417 0.05Fe-MCAC exhibited lower activation energy for the adsorption of naphthalene, 418 phenanthrene, and pyrene solutions that that of CAC. The CAC modified with iron nitrate 419 420 via microwave radiation was an efficient adsorbent of PAHs from aqueous solutions. The modified sample also showed good stability and reusability for the adsorption of PAHs in 421 solutions. Thus, the CAC sample modified via a simple treatment is a very effective sorbent. 422

423

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